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## CHEMICAL CORPS

# CONSOLIDATED R&D ANNUAL PROJECT REPORT

(EXCLUDING GM) (REPORTS CONTROL SYMBOL CSCRD-16)

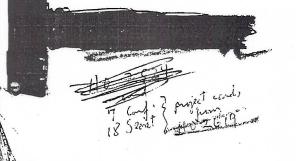
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Vol 1
31 December 1957



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EPORT DATE	CW Agent Process Development	(U)		The second second		4-92-03-013
Dec 57	0,, 2-8	.1		4. INDEX NUMBER		5. REPORT DATE
		4				31 Dec 57
	A BASIC FIELD OR SUBJECT	7. SUB FIELD O	R SUBJECT SUB GE	ROUP		7A. TECH. OBJ.
	Processing & Manufacturing	2				
sibility	Methods & Techniques & Equipment	111	Chemical			CW-la
preparing	B. COGNIZANT AGENCY		R AND/OR LABORA	TORY	CONTRA	CT/W. O. NO.
ugway	CmlC	Proc Dev	Div, Dir	Dev,		
	9. DIRECTING AGENCY	USA CW				
	CmlC R&D Cmd		nieson Che	m Corn	DAU1!	8-108-CML-6109
51 thru 53,	10. REQUESTING AGENCY				1	
ects,	CmlC	Corp.	chinery an	d Chem	and	8-108-CML-5725
54.) Liai-	11. PARTICIPATION AND/OR COORDINATION	13. RELATED PR	OJECTS			COMPLETION DATES
hemical	(47)	4-04-15	022		RES.	
This	Army (AR)	4-04-15	-032		DEV.	Cont.
District					TEST	Cont.
	<u>.</u>				OP. EVAL	
iteria					18. FY.	FISCAL ESTIMATES
d on the	\$ 5.50 1.50 1.50 1.50 1.50 1.50 1.50 1.50	14. DATE APPRO	VED		58	936M
2 ou rue		9 Dec 54,	CCTC Ite	m 2962	59	360M
	·	15. PRIORITY	16. MAJOR CATEG	ORY	60	360M
		1-B	52		Cont	inuing rate
	19. REPLACED PROJECT CARD AND PROJECT STATUS Subproject card 4-92-03-013-02	datad 21	Dec 561		p/a	980M
	CCTC Item 3388, 12 Dec 57.	, dated 31	Dec. 50;	revised		
	20. FIREMENT AND/OR JUSTIFICATION					
	There is a requirement for	the develo	pment of	CW agents.	Nec	essary steps
	between research and the ult	imate pro	duction fr	om CmlC	acilit	ies are the
	development of chemical pro	_				
	pilot plants based on such pr	i.	_			-
	equipment design data through					
	of agents for field evaluation				-	
	ref. par. 1212a.	or agent	and disser	iimațion te	cımıdı	ies. CDOG
	21. BRIEF OF OJECT AND OBJECTIVE			· · · · · · · · · · · · · · · · · · ·		,
	Brief. (Applied Resear	ch) The c	bject of the	nis project	is: C	peration of a
	chemical-process labor	atory for	the develo	pment of p	roces	s data and
	process-control techniq	ues; desig	n, constr	uction and	opera	tion of pilot
	plants to develop proces	_				_
	production of agents for					
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y, funds	b. Approach. The approach	h taken in	Drocess	and product	+ 20116	lonment is:
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characteristics of reactants and reactions leading to an end process or product.

- (2) Select a sound technical and economical process for development.
- (3) Develop the controls necessary for sound technical and economic processing.
- (4) Develop data for the design of piloting facilities,
- (5) Design and build piloting facilities for processing facilities.
- (6) Operate pilot plants to develop and furnish complete processing information, engineering data and process products for use in further development.
- c. Subprojects and/or Tasks.
  - (1) Process Development Studies
  - V-Agent Pilot-Plant Studies
- d. (U) Fiscal Estimates:

Period	Total Estimate	Army R&D Funds	Proc & Prod Funds	Other Ident. Army Funds	Other Agency Funds
FY55-57	: 3406M	2990M	415M	1M(ORD)	.⇔O⇔
FY58	1317M	936M	360M	10M(ORD) 11(0&M)	⇔0.∞
T	47.23M	3926M	775M	22M	<b>40</b> -

Other Information. None.

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Background History and Progress.

) Background History.

This project previously included subprojects 4-92-03-013-02, CW Agent Process Development; 4-92-03-013-03, CW Agent Filling Equipment Development; and 4-09-03-013-04 Smokes & Incendiaries. CCTC Item 3388, dated 12 Dec 57, revised this project by continuing subproject 4-09-03-013-02 as project 4-09-03-013. Work under 4-09-03-013-03 was continued as subproject 4-04-15-032-06 and subproject 4-09-03-013 was suspended.

(a) G Agents. In 1947 GB was selected as the G agent to be produced for general field use, and the DMHP process was also selected as the most satisfactory for the production of GB. Based upon pilot-plant development, production facilities were designed, constructed and operated.

Since 1951 several additional processes for the production of GB have been investigated. The process that offers the most advantages is a high temperature method (HTM process) of combining methane with phosphorous trichloride to form dichlormethylphosphine.

(b)(3):10 USC 130,(b)(2) HIGH

(b) V Agents.

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Process development work was begun both in these Laboratories and by Olin Mathieson Corporation under contract DA-18-108-CML-6109. Process data developed by these sources were applied to pilot-plant design as fast as available.

(C)

A source of the organic phosphorus intermediate, dichlormethylphosphine, existed in the pilot plant built and operated by Westvaco Chlor-Alkali Division, Food Machinery and Chemical Corporation under contracts DA-18-108-CML-5725 and DA-18-108-CML-5726. This source proved to be limited to 22, 500 lb. of the crude intermediate, which was purchased, and purification equipment was built at these Laboratories to further refine the material to a grade usable in the transester process.

(S)

Progress.

(a) Process Development Studies of V Agent.

(1) Dichlormethylphosphine. Process and pilot-plant development was done by Westvaco Chlor-Alkali Division of Food Machinery Corporation under contracts DA-18-108-CML-5725 and DA-18-108-CML-5726 for the HTM process. Pilot-plant development work has been completed; unit-plant design phase is incomplete.

(C)

Step I. Investigation of the process variables was continued in the process laboratory and under contract DA-18-108-CML-6109 by Olin Mathieson Corporation.

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Emphasis and most of the work has been directed toward the development of continuous process equipment and process controls.

The related problems of process control and analytical methods in this and in succeeding reaction steps are being worked on by processing-laboratory personnel. The many problems in these areas cannot be solved by effort of these Laboratories alone in the time available. Assistance will be obtained from industry under a contract, as described below.

- Step II. Investigation of the reactions in this step of the process have been continued in the process laboratory on both bench scale and prepilot-plant scale. The work has generally been done by a batch process and has been directed specifically toward a study of separation methods for the reaction components and purification methods for the transester end product. Here as in Step I, progress will be accelerated by solution of the problems of process control and analytical methods.
- (4) Step III. In this step of the process, sulfur is added to transester followed by isomerization to produce VX. A small-scale, 8 lb. per batch, process has been developed to produce agent for munitions and dissemination development. Approximately 1000 lb. of agent has been so produced for these purposes. The process work has served as a basis for the design of the pilot-plant reactor system.
- (5) Contract Proposal. Additional research and development is urgently needed in the determination of physical and chemical characteristics of reactants and reactions, in analytical methods for both process-stream constituents and intermediates. These are the first tasks proposed in the contract, and will be followed by a task to develop

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industrial firms, incleading engineering organizate proposed work. The written and submitted Chemical Center Pro	
(b) V-Agent Pilot-Plant Studi	
unit to produce and pu 1000 lb. of dichlorme will produce material	been completed on an HTM process urify by distillation approximately ethylphosphine every 24 hr. This unit l of approximately 95% purity as feed pilot plant. Design of the agent pilot
plant is complete. Cl additional process inf process laboratory, o	hanges in design are being made as formation becomes available from the or from operation of the pilot plant
itself.	f. (S
Operation of this unit Construction of Step I	ruction of the HTM unit is underway. is scheduled for 4th Q FY 58. and Step II pilot facilities have been n of Step III is scheduled for 3rd Q
(3) Operation.	
( <u>a</u> ) (b)(2) HIGH	
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	of this step in the pilot plant has lesigned it is continuous. Deposition

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of the solid ammonium chloride on reactor heat-transfer surfaces has so far limited the continuity of operation to 48 hr., or less. Purification equipment operated satisfactorily. The material produced was shown, by assay at the process laboratory, to be satisfactory. Other types of continuous reactors are being tried in the search for an answer to the ammonium chloride problem.

- (c) Step II. Operation of this piloting equipment has been started. Some minor changes in design and construction have been made to correct deficiencies made apparent by the limited operation.
- Operation of this final step in the process is (d) Step III. scheduled for the 3rd Q FY 58.

## Future Plans.

- (1) Expedite the development, by contract and CWL effort, of basic data in the areas of process data, analytical methods, and process control.
- (2) Complete the construction of the HTM unit and Step III pilot facilities. Completion of the HTM unit will permit operation of the agent pilot plant unrestricted by inadequate supply of dichlormethylphosphine.
- (3) Continue operation of the agent pilot plant and complete process development.

### References.

(1) CWL Technical Memorandum 31-6, Agent 1701 - Comparison of the Transester Process and a Water-Wash Process for Production -Preliminary Report, 21 January 1957.

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- (2) CWL Technical Memorandum 31-15, Preliminary Report on V-Agent Pilot Plant Section 5: Step O Process Detail, 14 February 1957.
- (3) CWL Technical Memorandum 31-16, Process Laboratory Development of Transester Process, Step 1, February 1957.
- (4) CWL Technical Memorandum 31-23, Preliminary Report on V-Agent Pilot Plant, Part 2: Step O Data Book, I March 1957.
- (5) CWL Technical Memorandum 31-24, Preliminary Report on V-Agent Pilot Plant. Part 2: Step I Data Book, 1 April 1957.
- (6) CWL Technical Memorandum 31-25, Preliminary Report on V-Agent Pilot Plant. Section 5: Step I Process Details, 8 April 1957.
- (7) CWL Technical Memorandum 31-26, Reaction of ROH with Methyldichlorphosphine Without an Acid Acceptor, 12 April 1957.
- (8) CWL Technical Memorandum 31-27, Preliminary Report on V-Agent Pilot Plant. Section V: Step II Process Details, 1 May 1957.
- (9) CWL Technical Memorandum 31-30, Preliminary Report on V-Agent Pilot Plant. Part 3: Process and Engineering Program Step I, 17 June 1957.
- (10) CWL Technical Memorandum 31-35, Prepilot Evaluation of Size O Turba-Film Evaporator, August 1957.
- (11) CWL Technical Memorandum 31-41, Preliminary Report on V-Agent Pilot Plant, Part I, Section 5: Step 3 Process Details; and Part 3, Process Engineering Program, 5 September 1957.
- (12) CWL Technical Memorandum 31-42, Preliminary Report on V-Agent Pilot Plant. Part II; Step 2 Data Book, September 1957.

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- (13) CWL Technical Memorandum 31-43, Preliminary Report on V-Agent Pilot Plant. Part II: Step 3 Data Book, 18 September 1957.
- (14) CWL Technical Memorandum 31-44, Report on Modified HTM Plant. Section 5: HTM Process Details, September 1957.
- (15) CWL Technical Memorandum 31-45, Preliminary Report on V-Agent Pilot Plant. Part III: Process and Engineering Program Step II, 8 October 1957.
- (16) CWL Technical Memorandum 31-51, Pilot Plant Process and Engineering Reports on Agent EA 1701 by the Transester Process, 31 October 1957.
- (17) Olin Mathieson Chemical Corp., Final Report on DA-18-108-CML-6109, Project Gibraltar, 1 September 1957.
- (18) Food Machinery and Chemical Corp., Final Report on DA-18-108-CML-5725, Development of HTM Pyro Process, June 1957.

## Modernization Code.

Not applicable.

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